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IN THE CLAIMS

- 1. (Withdrawn) A fuel system comparising:
 a fuel storage tank;
 a downstream use for fuel;
 a fluid connection for con
 downstream use; and
- a fuel deoxygenator mounted for their connection, said fuel deoxygenator having a non-porous membrane, said non-porous membrane layer and at least a second membrane layer disposed on top of said first membrane layer.
- 2. (Withdrawn) The fuel system as recited in claim 1, wherein said non-porous membrane is disposed on a substrate.
- 3. (Withdrawn) The fuel system as recited in claim 1, wherein at least one of said first membrane layer and said second membrane layer is a fluoropolymer.
- 4. (Withdrawn) The fuel system as recited in claim 3, wherein at least one of said first membrane layer and said second membrane layer is an amorphous glassy perfluorodioxole copolymer.
- 5. (Withdrawn) The fuel system as recited in claim 1, wherein said non-porous membrane is a homogenous non-porous membrane.
- 6. (Currently Amended) A method of manufacturing preventing a liquid from migrating into a non-porous membrane device comprising the steps of:

forming a first membrane layer in a first coating process by drying a first solution in a first drying process;

forming a second membrane layer on top of the first membrane layer in a second coating process by drying a second solution in a second drying process, the second membrane layer and the first membrane layer form a non-porous membrane; and

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disposing said non-porous membrane in a fluid separating device.

- 7. (Original) The method as recited in claim 6, including the step of disposing the non-porous membrane on a substrate.
- 8. (Original) The method as recited in claim 6, including the step of forming a partially dissolved portion of the first membrane layer by partially dissolving the first membrane layer with the second solution so that the second membrane layer forms a single homogenous non-porous membrane with the first membrane layer after the second drying process.
- 9. (Original) The method as recited in claim 6, wherein the first solution comprises an amorphous glassy perfluorodioxole copolymer dissolved in a fluorosolvent that has a boiling point between 60°C and 110°C.
- 10. (Original) The method as recited in claim 6, wherein the second solution comprises an amorphous glassy perfluorodioxole copolymer dissolved in a fluorosolvent that has a boiling point between about 60°C and about 110°C.
- 11. (Original) The method as recited in claim 6, wherein said first drying process includes the step of heating to between about 130°C and about 150°C for between 10 minutes and about 30 minutes.
- 12. (Original) The method as recited in claim 6, wherein said second drying process includes the step of heating to between about 130°C and about 150°C for between 10 minutes and about 30 minutes.
- 13. (Original) The method as recited in claim 6, wherein said first coating process includes rolling said first solution onto said substrate.
- 14. (Original) The method as recited in claim 6, wherein said second coating process includes rolling said second solution on top of said first membrane layer after said first drying process.

- 15. (Original) The method as recited in claim 6, wherein said fluid separating device is a fuel deoxygenator of an aircraft.
- 16. (Currently Amended) A fluid separator comprising:

 having a first membrane layer; and at least
 a second membrane layer disposed on top of said first membrane layer; and
 an indistinct, seamless boundary between the first membrane layer and the second
 membrane layer.
- 17. (Original) The fluid separator as recited in claim 16, wherein said fluid separator is disposed on a substrate.
- 18. (Original) The fluid separator as recited in claim 16, wherein at least one of said first membrane layer and said at least a second membrane layer is formed from a fluoropolymer.
- 19. (Original) The fluid separator as recited in claim 18, wherein at least one of said first membrane layer and said at least a second membrane layer is formed from an amorphous glassy perfluorodioxole copolymer.
 - 20. (Cancelled)
- 21. (New) The fluid separator as recited in claim 16, wherein the first layer is a first-formed layer and the second layer is a later-formed later relative to the first-formed layer.
- 22. (New) The fluid separator as recited in claim 16, wherein the first membrane layer and a second membrane layer each include a thickness of about one micrometer.
- 23. (New) The method as recited in claim 6, further comprising forming the first membrane layer with a thickness of about one micrometer and forming the second membrane layer with a thickness of about one micrometer.

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- 24. (New) The method as recited in claim 6, wherein the first drying process occurs before the second coating process.
- 25. (New) The method as recited in claim 6, further comprising forming a seamless boundary between the first membrane layer having a thickness of about one micrometer and the second membrane layer having a thickness of about one micrometer.
- 26. (New) The method as recited in claim 6, wherein the first solution and the second solution are equivalent to form the first membrane layer and the second membrane layer of a single type of polymer.